#### **Basic control actions**

- A controller compares the actual value of output with the reference input, determines the deviation, and produces a control signal that will reduce the deviation to zero or to a small value.
- The manner in which the controller produces the control signal is called the *control action*.

## block diagram of an industrial control system



# Classifications of Industrial Controllers.

- 1. Two-position or on-off controllers
- 2. Proportional controllers
- 3. Integral controllers
- 4. Proportional-plus-integral controllers
- 5. Proportional-plus-derivative controllers
- 6. Proportional-plus-integral-plus-derivative controllers

#### **Proportional Control of Systems.**



$$u(t) = K_p e(t) \qquad \qquad \frac{U(s)}{E(s)} = K_p$$

$$\frac{E(s)}{R(s)} = \frac{R(s) - C(s)}{R(s)} = 1 - \frac{C(s)}{R(s)} = \frac{1}{1 + G(s)}$$

$$E(s) = \frac{Ts + 1}{Ts + 1 + K} \frac{1}{s}$$

$$e_{ss} = \lim_{t \to \infty} e(t) = \lim_{s \to 0} sE(s) = \lim_{s \to 0} \frac{Ts + 1}{Ts + 1 + K} = \frac{1}{K + 1}$$

 Such a system always has a steady-state error in the step response. Such a steady-state error is called an offset.



## Integral Control of Systems.



Integral control of the system eliminates the steady-state error in the response to the step input..

## Response to Torque Disturbances (Proportional Control)

Assuming that the reference input is zero or R(s) = 0, the transfer function by C(s) and D(s) is given by

$$\frac{C(s)}{D(s)} = \frac{1}{Js^2 + bs + K_p}$$



Hence

$$\frac{E(s)}{D(s)} = -\frac{C(s)}{D(s)} = -\frac{1}{Js^2 + bs + K_p}$$

The steady-state error due to a step disturbance torque of magnitude  $T_d$  is given by

$$e_{ss} = \lim_{s \to 0} sE(s)$$
$$= \lim_{s \to 0} \frac{-s}{Js^2 + bs + K_p} \frac{T_d}{s}$$
$$= -\frac{T_d}{K_p}$$
T

$$c_{ss} = -e_{ss} = \frac{T_s}{K_p}$$

## Response to Torque Disturbances (Proportional-Plus-Integral Control

- To eliminate offset due to torque disturbance, the proportional controller may be replaced by a proportional-plus-integral controller.
- If integral control action is added to the controller, then, as long as there is an error signal, a torque is developed by the controller to reduce this error, provided the control system is a stable one.

The closed-loop transfer function between C(s) and D(s) is

$$\frac{C(s)}{D(s)} = \frac{s}{Js^3 + bs^2 + K_ps + \frac{K_p}{T_i}}$$

In the absence of the reference input, or r(t) = 0, the error signal is obtained from

$$E(s) \approx -\frac{s}{Js^3 + bs^2 + K_ps + \frac{K_p}{T_i}}D(s)$$



If this control system is stable, that is, if the roots of the characteristic equation

$$Js^{3} + bs^{2} + K_{p}s + \frac{K_{p}}{T_{i}} = 0$$

have negative real parts, then the steady-state error in the response to a unit-step disturbance torque can be obtained by applying the final-value theorem as follows:

$$e_{ss} = \lim_{s \to 0} sE(s)$$
$$= \lim_{s \to 0} \frac{-s^2}{Js^3 + bs^2 + K_ps + \frac{K_p}{T_i}} \frac{1}{s}$$
$$= 0$$

It is important to point out that if the controller was an integral controller, then the system always becomes unstable because the characteristic equation

 $Js^3 + bs^2 + K = 0$ 

will have roots with positive real parts. Such an unstable system cannot be used in practice.

#### **Proportional-Plus-Derivative Control**



. Thus derivative control introduces a damping effect. A typical response curve *c* (*t*) to *a unit step* input is shown in

 Effect of Proportional, Integral & Derivative Gains on the Dynamic Response

## Change in gain in P controller



- Increase in gain:
  - $\rightarrow$  Upgrade both steady
    - state and transient

responses

- → Reduce steady-state error
- → Reduce stability!

## P Controller with *high* gain



## Integral Controller

Integral of error with a constant gain

 → increase the system type by 1
 → eliminate steady-state error for
 a unit step input
 → amplify overshoot and oscillations

#### Change in gain for PI controller



- Increase in gain:
  - → Do not upgrade steadystate responses
     → Increase slightly
    - settling time
  - → Increase oscillations and overshoot!

#### **Derivative Controller**

Differentiation of error with a constant gain

 → detect rapid change in output
 → reduce overshoot and oscillation
 → do not affect the steady-state response

# Effect of change for gain PD controller



- Increase in gain:
  - $\rightarrow$  Upgrade transient

response

- → Decrease the peak and rise time
- → Increase overshoot and settling time!

#### Changes in gains for PID Controller



Ziegler-Nichols rules for tuning PID controllers.

- These rules are used to determine Kp, Ti and Td for PID controllers
- First Method: The response is obtained experimentally to a unit step input. The plant involves neither integrators nor differentiators





- (u) - - -

Ziegler and Nichols suggested to set the values of  $K_p$ ,  $T_i$ , and  $T_d$ 

according to Table 10-1.

Table 10-1 Ziegler-Nichols Tuning Rule Based on Step Response of Plant (First Method)

Type of Controller	$K_p$	Ťi	$T_d$
Р	$\frac{T}{L}$	œ	0
PI	$0.9 \frac{T}{L}$	$\frac{L}{0.3}$	0
PID	$1.2\frac{T}{L}$	2 <i>L</i>	0.5 <i>L</i>

## Second Method

- Set Ti= inf and Td=0, increase Kp from 0 t a critical value Kcr where the output exhibits sustained oscillations.
- Use Kcr , Pcr and Table 10-2 to determine the parameters of the controller





#### **Table 10–2** Ziegler–Nichols Tuning Rule Based on Critical Gain $K_{cr}$ and Critical Period $P_{cr}$ (Second Method)

Type of Controller	$K_p$	$T_i$	$T_d$
Р	0.5 <i>K</i> <sub>cr</sub>	8	0
PI	0.45K <sub>cr</sub>	$\frac{1}{1.2}\mathbf{P_{cr}}$	0
PID	0.6K <sub>cr</sub>	0.5 <i>P</i> <sub>cr</sub>	0.125P <sub>cr</sub>